

# Selective Catalytic Reduction of NO<sub>x</sub> using Hydrocarbon



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**Doctor of Philosophy**

By

*Deepak Yadav*

DEPARTMENT OF CHEMICAL ENGINEERING  
INDIAN INSTITUTE OF TECHNOLOGY  
(BANARAS HINDU UNIVERSITY)  
VARANASI- 221005

Roll No. 13041001

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**CHAPTER – 6**

**CONCLUSIONS**

**AND**

**FUTURE SCOPE**



## CONCLUSIONS

Based on the experimental results and discussion following conclusions can be drawn:

- Spinel catalysts ( $\text{MnCo}_2\text{O}_4$ ,  $\text{CuCo}_2\text{O}_4$ ,  $\text{NiCo}_2\text{O}_4$ ) are prepared by different methods (CP, NC, DCP) for comparative studies of SCR of NO using  $\text{H}_2$ - $\text{C}_3\text{H}_8$  reductant.
- The order of preparation methods of the catalysts for NO reduction activity was as follows:  $\text{NC} \approx \text{DCP} > \text{CP}$ .
- The order of calcination strategies of catalyst precursors for SCR of NO activity was as follows:  $\text{RC} > \text{FA} > \text{SA}$ .
- The order of unsupported catalyst based on activity for the reaction follows the following trend:  $\text{MnCo}_2\text{O}_4 > \text{CuCo}_2\text{O}_4 > \text{NiCo}_2\text{O}_4$ .
- The optimum loading of  $\text{MnCo}_2\text{O}_4$  on  $\gamma\text{-Al}_2\text{O}_3$  is 32%.
- The performance order of promoted and supported catalysts for SCR of NO using  $\text{H}_2$  assisted  $\text{C}_3\text{H}_8$  is as follows:  $0.2\% \text{Rh}32\% \text{MnCo}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3 > 0.3\% \text{Rh}32\% \text{MnCo}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3 > 0.1\% \text{Rh}.32\% \text{MnCo}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3$ .
- The catalyst formulation,  $0.2\% \text{Rh}32\% \text{MnCo}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3$  (Cat-K) prepared by DCP followed by RC route of calcination shows the best NO-SCR performance with  $\text{H}_2$ - $\text{C}_3\text{H}_8$  reductant, 98.8% NO conversion was achieved at  $147^\circ\text{C}$ .
- The kinetics of NO-SCR over Cat-K is 1<sup>st</sup> order w.r.t. NO and the value of activation energy is found to be 93.82 kJ/gm mol and the rate of NO reduction is given by rate:  $(-r_p) = 14.78 \times 10^{10} \exp(-93820/RT)(C_{\text{NO}})$  gm mol/gm cat-h.

- H<sub>2</sub>-LPG (~72% C<sub>3</sub>H<sub>8</sub>) was used as reductant showed comparable SCR performance of NO to H<sub>2</sub>-C<sub>3</sub>H<sub>8</sub>. Therefore, with so many advantages of LPG, it is suggested to be used as reductant for SCR of NO<sub>x</sub> from vehicular exhaust. Care should be taken to eliminate mercaptane content of LPG to prevent deactivation of the catalyst. The mercaptane content in LPG is ~ 30 ppm. Therefore, the feed stream containing LPG reductant should be made free of mercaptane by bubbling it through a solution of sodium plumbite.

### • FUTURE SCOPE

- There are more than hundreds of publication on C<sub>3</sub>H<sub>8</sub> reductant for SCR of NO. A typical composition of LPG (74.23% C<sub>3</sub>H<sub>8</sub>, 13.03% n-C<sub>4</sub>H<sub>10</sub>, 12.19% i-C<sub>4</sub>H<sub>10</sub> and 0.55% C<sub>2</sub>H<sub>6</sub>) used as reductant shows comparable SCR performance of NO to C<sub>3</sub>H<sub>8</sub>. Therefore, with so many advantages of LPG, it is suggested for future applications.
- Kinetics studies for SCR of NO using LPG reductant should be performed.
- Effect of water vapours and SO<sub>2</sub> deactivation can be studied on the catalyst, in order to commercialize it for lean burn diesel NO<sub>x</sub> abatement.