

## List of Figures

<b>Figure No</b>	<b>Figure Caption</b>	<b>Page No</b>
<b>Figure 1.1</b>	Water distribution across the world	2
<b>Figure 1.2</b>	Classification of technologies available for pollutant removal	3
<b>Figure 1.3</b>	Membrane separation process classification based on their pore size and pressure.	7
<b>Figure 1.4</b>	Number of publications from 2008-2018 on the membrane technology for wastewater treatment	8
<b>Figure 1.5</b>	Current and proposed treatment method for removal of heavy metal	14
<b>Figure 2.1</b>	Schematic representation for green route synthesis of nanoparticles	23
<b>Figure 2.2</b>	Mechanism for photocatalytic degradation of pollutant	29
<b>Figure 2.3</b>	Different techniques for remediation of chromium contaminated water	42
<b>Figure 2.4</b>	Schematic representation of nanofiltration photocatalytic membrane	48
<b>Figure 2.5</b>	Experimental setup representation for As removal	49
<b>Figure 2.6</b>	Schematic representation of photocatalytic membrane reactor	51
<b>Figure 3.1</b>	Schematic representation of (a) particle and (b) membrane synthesis	88
<b>Figure 3.2</b>	(a) HRTEM image of TiO <sub>2</sub> NPs (b) SAED pattern of TiO <sub>2</sub> NPs	93
<b>Figure 3.3</b>	(a) XRD pattern (b) DLS spectra of synthesized TiO <sub>2</sub> NPs (c) XRD pattern of TiO <sub>2</sub> NPs , PVDF and PVDF/ TiO <sub>2</sub> membrane	94
<b>Figure 3.4</b>	(a) FTIR spectra and (b) Fraction value of $\alpha$ and $\beta$ -phases of pure PVDF and PVDF/TiO <sub>2</sub> composite membranes	96
<b>Figure 3.5</b>	(a) DRS spectrum (b) Band energy of PVDF/TiO <sub>2</sub> composite membranes	97
<b>Figure 3.6</b>	Ternary Phase diagram of PVDF/NMP (a) no TiO <sub>2</sub> (b) 1 wt% TiO <sub>2</sub> (c) 2 wt% TiO <sub>2</sub> (d) 3 wt% TiO <sub>2</sub>	98
<b>Figure 3.7</b>	(a) Relative concentration versus time	100
<b>Figure 3.7</b>	(b) Relative concentration versus $t^{0.5}$ for different composite membranes	101

<b>Figure 3.7</b>	(c) Comparison of the thermodynamic and kinetic properties of the polymeric casting solution	103
<b>Figure 3.8</b>	HRSEM images (a) no TiO <sub>2</sub> (b) 1 wt% TiO <sub>2</sub> (c) 2 wt% TiO <sub>2</sub> (d) 3 wt% TiO <sub>2</sub>	104
<b>Figure 3.9</b>	Change in (a)Contact angle, (b) pore size,(c) porosity (d) tortuosity with TiO <sub>2</sub> loading	106
<b>Figure 4.1</b>	3D AFM image of different PVDF composite membranes.	123
<b>Figure 4.2</b>	Variation of interaction energy between membrane and BSA	127
<b>Figure 4.3</b>	Inhibition zone formation for different PVDF composites membrane	128
<b>Figure 4.4</b>	The OD <sub>600</sub> value of the PM1 (control, no TiO <sub>2</sub> ), PM2, PM3, and PM4 incubated for 24h.	129
<b>Figure 4.5</b>	HRSEM images of PVDF-TiO <sub>2</sub> membranes before and after bacterial growth.	130
<b>Figure 4.6</b>	Antibacterial activity of different composite membranes	131
<b>Figure 4.7</b>	(a) Water flux value for different composite membranes before and after filtration of BSA bearing water (b) FRR and (c) % BSA rejection for different PVDF/TiO <sub>2</sub> composite membrane (d) Flux ratio during filtration of HA solution.	134
<b>Figure 5.1</b>	The dead-end filtration cell	148
<b>Figure 5.2</b>	Adsorption capacity of composite membrane at different TiO <sub>2</sub> loading	153
<b>Figure 5.3</b>	Pure water flux before and after BSA filtration	154
<b>Figure 5.4</b>	a) FRR of membranes b) Fouling resistance of membranes	155
<b>Figure 5.5</b>	Comparison of experimental and predicted filtration data and classic fouling models for membrane	157
<b>Figure 6.1</b>	Schematic representation of setup for rejection of Cr(VI) using membrane and reduction of Cr(VI) using photocatalyst	167
<b>Figure 6.2</b>	Schematic representation of the mechanism from Cr(VI) removal	173
<b>Figure 6.3</b>	UV spectra of Cr(VI) solution at different condition	174
<b>Figure 6.4</b>	Effect of NPs loading: (a) Variation of Flux, (b) % rejection & (c) % reduction with time	176

<b>Figure 6.5</b>	Effect of particle size: (a) Variation of Flux, (b) %rejection and (c) % reduction with time	177
<b>Figure 6.6</b>	Effect of pH: Variation of (a) Flux, (b) %rejection and (c) % reduction with time	179
<b>Figure 6.7</b>	Effect of [Cr(VI)]: (a)Variation of Flux, (b) %rejection and (c) % reduction with time	180
<b>Figure 6.8</b>	Effect of transmembrane pressure: (a) Variation of flux, (b) % Rejection and % reduction with time	181
<b>Figure 6.9</b>	Actual vs. Predicted plot of model a) % Rejection b) % Reduction	182
<b>Figure 6.10</b>	3D dimensional response surface and contour plots of % Rejection showing the effect of (a) Particle Loading and Cr concentration (b) pH and Particle Loading; (c) pH and Cr concentration	185
<b>Figure 6.11</b>	3D dimensional response surface and contour plots of % Reduction showing the effect of (a) Particle Loading and Cr concentration (b) pH and Particle Loading; (c) pH and Cr concentration.	187
<b>Figure 6.12</b>	(a) Reusability of PVDF/TiO <sub>2</sub> membrane for Cr (VI) removal (b) Contact Angle value of the membrane after each run	189
<b>Figure 6.13</b>	FTIR spectra of membrane at different operating condition	190
<b>Figure 6.14</b>	BET surface area of membrane before and after Cr removal	190
<b>Figure 6.15</b>	Graph of pH, TSS, COD, and Cr for wastewater before and after treatment for 3 different types of tannery industry	192