| A | Area under the breakthrough curve |
| :---: | :---: |
| AAS | Atomic Absorption Spectroscopy |
| b | Langmuir constant related to the affinity of binding sites ( $\mathrm{L} / \mathrm{mg}$ ) |
| BDST | Bed Depth Service Time Model |
| BET | Brauner-Emmett-Teller |
| C | Intercept called boundary layer effect |
| $\mathrm{C}_{\text {AE }}$ | Equilibrium concentration of the solute on the adsorbent (mg/L) |
| $\mathrm{C}_{\text {ads }}$ | Adsorbed metal ion concentration |
| $\mathrm{C}_{\text {b }}$ | Breakthrough metal ion concentration |
| $\mathrm{C}_{\text {e }}$ | equilibrium concentration of the adsorbate ( $\mathrm{mg} / \mathrm{L}$ ) in batch mode |
| $\mathrm{C}_{\text {t }}$ | concentration of the adsorbate remaining after adsorption has taken place over a time period of $t(\mathrm{mg} / \mathrm{L})$, in batch mode |
| $\mathrm{C}_{\mathrm{t}}$ | effluent metal ion concentration ( $\mathrm{mg} / \mathrm{L}$ ) in continuous mode |
| $\mathrm{C}_{0}$ | initial adsorbate concentration |
| Conc. | concentration ( $\mathrm{mg} / \mathrm{L}$ ) |
| E | Mean free energy of the adsorption (kJ/mol) |
| e.g. | for example |
| et al. | and others |
| EDX | Energy Dispersive X-ray Analysis |
| FTIR | Fourier-transform infrared |
| i.e. | that is to say |
| h | hour |
| E\% | Elution efficiency |
| F | Polanyi potential |
| $\Delta \mathrm{G}$ | Gibbs free energy (kcal/mol) |
| GO | Graphene Oxide |
| h | initial sorption rate of pseudo second order kinetics of adsorption( $\mathrm{mg} / \mathrm{g} / \mathrm{min}$ ) |
| $\Delta \mathrm{H}$ | enthalpy change ( $\mathrm{kcal} / \mathrm{mol}$ ) |
| k | constant obtained by multiplying the $\mathrm{Q}^{\circ}$ and b (Langmuir's |
| constant) |  |
| $\mathrm{k}_{\mathrm{a}}$ | rate constant of BDST model ( $\mathrm{L} / \mathrm{mg} / \mathrm{min}$ ) |
| $\mathrm{K}_{\mathrm{F}}$ | Freundlich constant which indicate relative adsorption capacity $\left(\mathrm{mg}^{1-1 / \mathrm{n}} / \mathrm{gL}^{1 / \mathrm{n}}\right)$ |
| $\mathrm{k}_{\text {s }}$ | equilibrium rate constant of pseudo-first-order kinetics adsorption ( $\mathrm{min}^{-1}$ ) |
| $\mathrm{k}_{\text {id }}$ | rate constant of intraparticle diffusion ( $\mathrm{mg} / \mathrm{gh}^{0.5}$ ) |
| $\mathrm{K}_{\text {c }}$ | equilibrium constant |
| $\mathrm{k}_{\mathrm{L}}$ | column life factor |
| $k_{2}{ }^{\prime}$ | equilibrium rate constant of the pseudo-second-order kinetics of adsorption |
| m | mass of the adsorbent per unit of volume ( $\mathrm{g} / \mathrm{L}$ ) |
| M | adsorbate |
| MgO | Magnesium oxide |


| n | Freundlich constant indicative of the nature and strength of the adsorption process and the distribution of the adsorption sites |
| :---: | :---: |
| $\mathrm{N}_{\mathrm{b}}$ | bed volumes to breakthrough |
| $\mathrm{N}_{0}$ | Adsorption capacity of bed |
| nm | nanometre |
| ppm | parts per million |
| Q | Volumetric flow rate |
| $\mathrm{Q}^{\circ}$ | Langmuir constant represents the monolayer adsorption capacity ( $\mathrm{mg} / \mathrm{g}$ ) |
| q | uptake capacity of the nanoadsorbent (mg/g) |
| qe | amount of adsorbate adsorbed at equilibrium ( $\mathrm{mg} / \mathrm{g}$ ) |
| $\mathrm{q}_{\mathrm{m}}$ | amount of adsorbate adsorbed ( $\mathrm{mmol} / \mathrm{L}$ ) |
| $\mathrm{q}_{\mathrm{t}}$ | adsorption capacity of the adsorbent at time $\mathrm{t}(\mathrm{mg} / \mathrm{g})$ |
| $\mathrm{q}_{\text {tot }}$ | total adsorbed metal ion quantity (mg) |
| R | universal gas constant [8.314 J/mol/K] |
| $\mathrm{R}_{\mathrm{L}}$ | dimensionless separation constant |
| rpm | Rotation per minute |
| $\mathrm{R}^{2}$ | correlation coefficient |
| SEM | Scanning Electron Microscopy |
| $\Delta \mathrm{S}$ | Entropy change |
| T | Temperature |
| t | time |
| $\mathrm{tb}_{\text {b }}$ | breakthrough time (min) |
| $\mathrm{t}_{\mathrm{b}, \mathrm{i}}$ | initial breakthrough time (min) |
| $\mathrm{t}_{\mathrm{e}}$ | bed exhaustion or saturation time (min) |
| Temp. | temperature ( ${ }^{\circ} \mathrm{C}$ ) |
| u | linear velocity ( $\mathrm{cm} / \mathrm{min}$ ) |
| V | Volume of the solution (L) |
| $\mathrm{V}_{\text {eff }}$ | Effluent volume (L) |
| Vb | Volume of the solution treated at breakthrough time |
| W | Mass of the adsorbent |
| WHO | World Health Organization |
| Xm | maximum adsorption capacity of the adsorbent ( $\mathrm{mmol} / \mathrm{g}$ ) |
| XRD | X-Ray Diffraction |
| XPS | X-ray photoelectron spectroscopy |
| zpc | zero point charge |
| Z | Bed height (cm) |
| $\mathrm{Z}_{0}$ | Critical Bed Depth (cm) |
| $\mathrm{Z}_{0, \mathrm{i}}$ | initial critical bed depth (cm) |
| $\mathrm{ZrO}_{2}$ | Zirconium oxide |
| $\beta_{\mathrm{t}}$ | Mass transfer coefficient ( $\mathrm{cm} / \mathrm{sec}$ ) |
| $\beta$ | full width at half maximum |
| $\lambda$ | Wavelength |

