

NOMENCLATURE

A	Area, m ²
a	Radius of tube, m
C _p	Heat capacity, J/kg. K
D	Coil diameter, m
d	Tube diameter, m
D _h	Hydraulic diameter, m
e	Corrugation depth, m
F	Convective boiling enhancement factor
f	Friction factor
g	Acceleration due to gravity, m/s ²
G	Mass flux, kg/m ² s ¹
h	Heat transfer coefficient, W/m ² K
I	Current, A
L	Length, m
m	Mass flow rate, kg/s
N	Number of turns
N _d	Liquid gas density ratio
O	Volumetric flow rate, m ³ /s
p	Helical pitch, m
ΔP	Pressure drop across test section, N/m ²
q	Heat flux, W/m ²
Q	Heat transfer rate, W
S	Nucleate boiling suppression
ΔT	Difference in temperature, °C
T	Temperature, °C
u	Velocity, m/s
V	Voltage, V
X	Lockhart Martinelli parameter
x	Quality

Dimensionless Numbers

Bo	Boiling number, $Bo = q/G\gamma$
Co	Confinement number, $Co = \left(\frac{\sigma}{g(\rho_l - \rho_v)d_i^2} \right)^{0.5}$
De	Dean number, $De = Re\sqrt{\delta}$
F _d	Froude number, $F_d = Fr\sqrt{\delta} \cdot (1 + \tan \beta)^{0.2}$, $Fr = G^2 / \rho^2 gd$
Gr	Grashoff number, $Gr = \frac{g\alpha(T - T_b)d^3}{(\mu / \rho)^2}$
Gn	Germano number, $Gn = Re \left(\frac{(D/d)}{[\pi(D/d)]^2 + (p/d)^2} \right)$
He	Helical number, $He = De \left[1 + \left(\frac{p}{2\pi D} \right)^2 \right]^{1/2}$
Nu	Nusselt number, $Nu = \frac{h.d_i}{k}$
Pr	Prandtl number, $Pr = \frac{Cp \cdot \mu}{k}$
Ra	Rayleigh number, $Ra = Gr \cdot Pr$
Re	Reynolds number, $Re = \frac{d_i u \rho}{\mu}$

Greek Symbols

ϕ	DC power, W
ρ	Density, Kg/m ³
k	Thermal conductivity, W/mK
μ	Viscosity, N/m ² s
φ	Volume concentration
σ	Surface tension, Pa.s
δ	Curvature ratio, $\delta = d / D$
τ	Torsion ratio, $\tau = p^2 / ((D/2)^2 + p^2)$
ϕ_L	Pressure drop multiplier

α	Coefficient of thermal expansion
β	Dimensionless parameter
γ	Latent heat of evaporation, J/kg

Subscripts

b	Bulk
bf	Base fluid
c	Coil
crit	Critical
eq	Equivalent diameter
f	Fluid
i	Inner
in	Inlet
L	Laminar
l	Liquid
nf	Nanofluid
o	Outer
opt	Optimum
out	Outlet
Reg	Regression
s	Straight
tp	Two phase
t	Tube
T	Turbulent
v	Vapour
w	Wall